

触媒層内液水飽和モデルの開発

杵淵 郁也

東京大学 大学院工学系研究科 機械工学専攻

シミュレーションGr(京都大学 河瀬GL)事業内容説明会

2025年1月29日 NEDO川崎23F 2304会議室

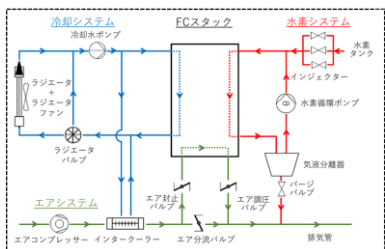


固体高分子形燃料電池内の物質輸送解析

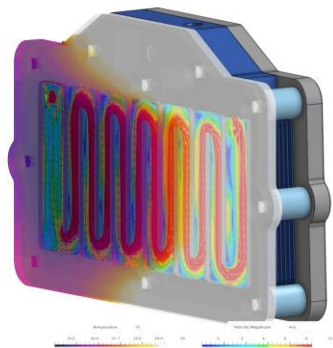
1

Multi-physics

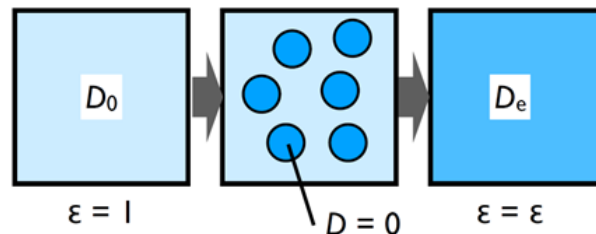
FC•DynaMo



<https://www.ch.t.kyoto-u.ac.jp/ja/information/laboratory/3koza/fc-dynamo>



<https://www.simscale.com/blog/hydrogen-fuel-cell-simulation-and-modeling/>



Bruggeman correlation

[V. D. Bruggeman, Ann. Phys., 1935]

$$\frac{\epsilon}{\tau} = \frac{D_e}{D_0} = \epsilon^a$$

$a=1.5$ (spheres)
 $a=2$ (cylinders)

$$\Omega(\{\rho\}) = k_B T \sum_i [\rho_i \ln \rho_i + (1 - \rho_i) \ln(1 - \rho_i)] V_i$$

Ideal Gas Contribution

$$-\frac{\epsilon_{ff}}{2} \sum_i \sum_{a \leq r_c} \rho_{i+a} \rho_i V_i$$

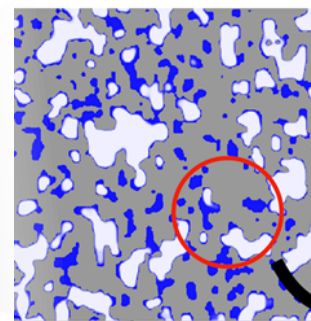
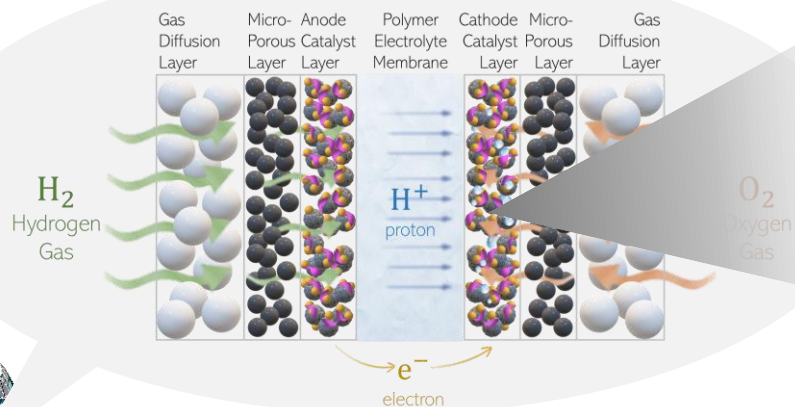
Fluid-Fluid Interaction

$$-\epsilon_{sf} \sum_i \sum_{|a| \leq r_c} \chi(i, a) \rho_i V_i$$

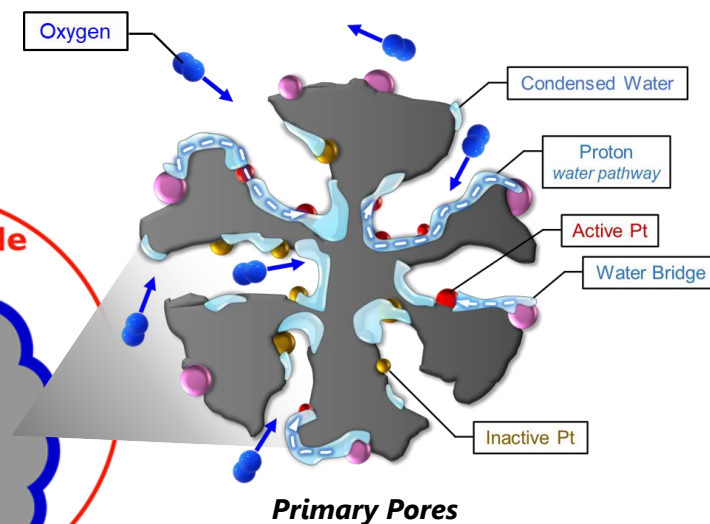
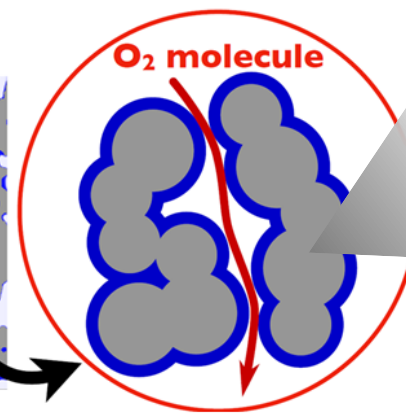
Solid-Fluid Interaction

$$-\sum_i \mu \rho_i V_i$$

Chemical Potential

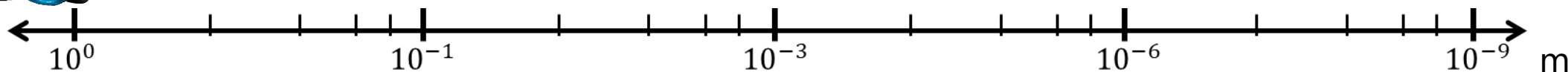


Secondary Pores

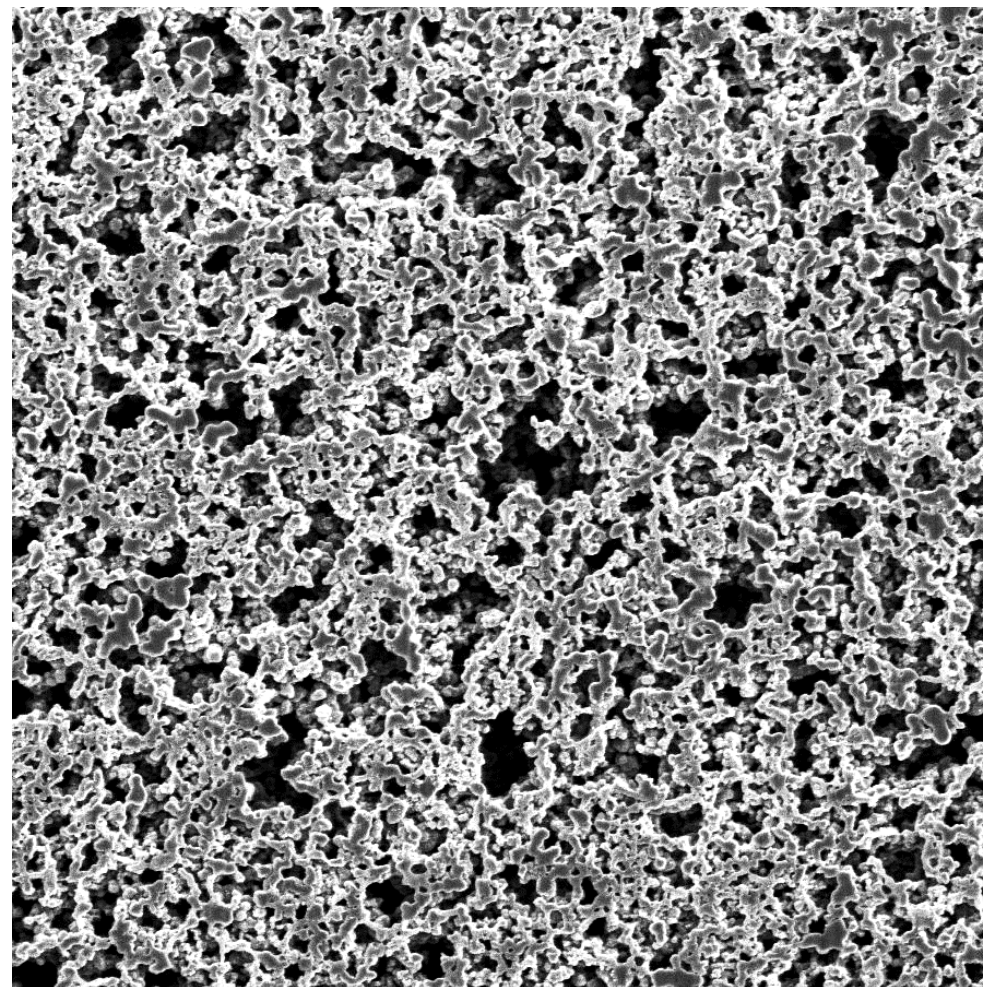


Primary Pores

Multi-scale

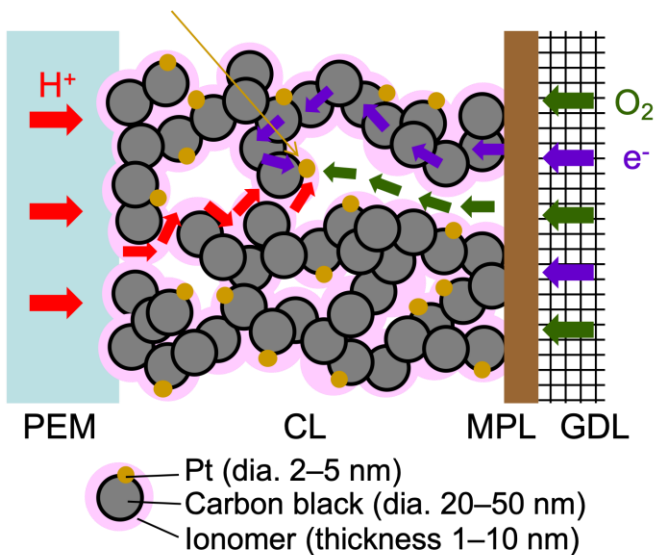
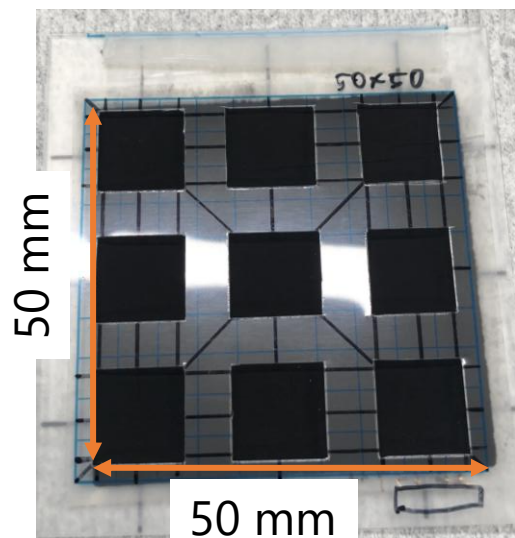
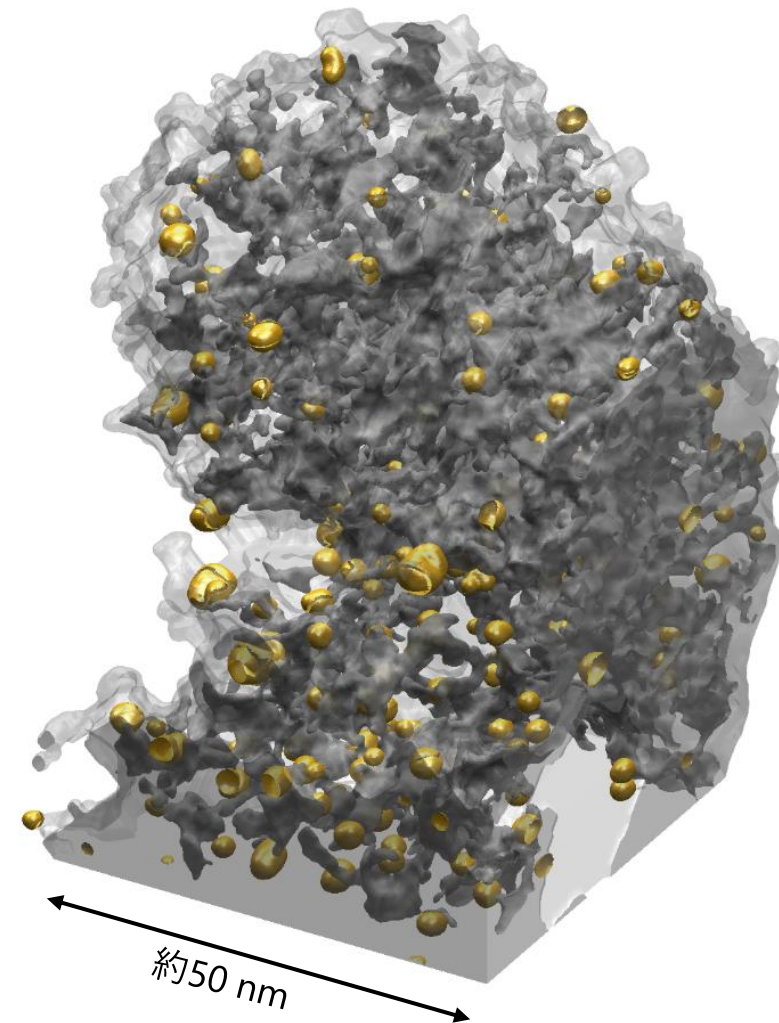


● FIB-SEM連続断面像 (二次細孔構造)



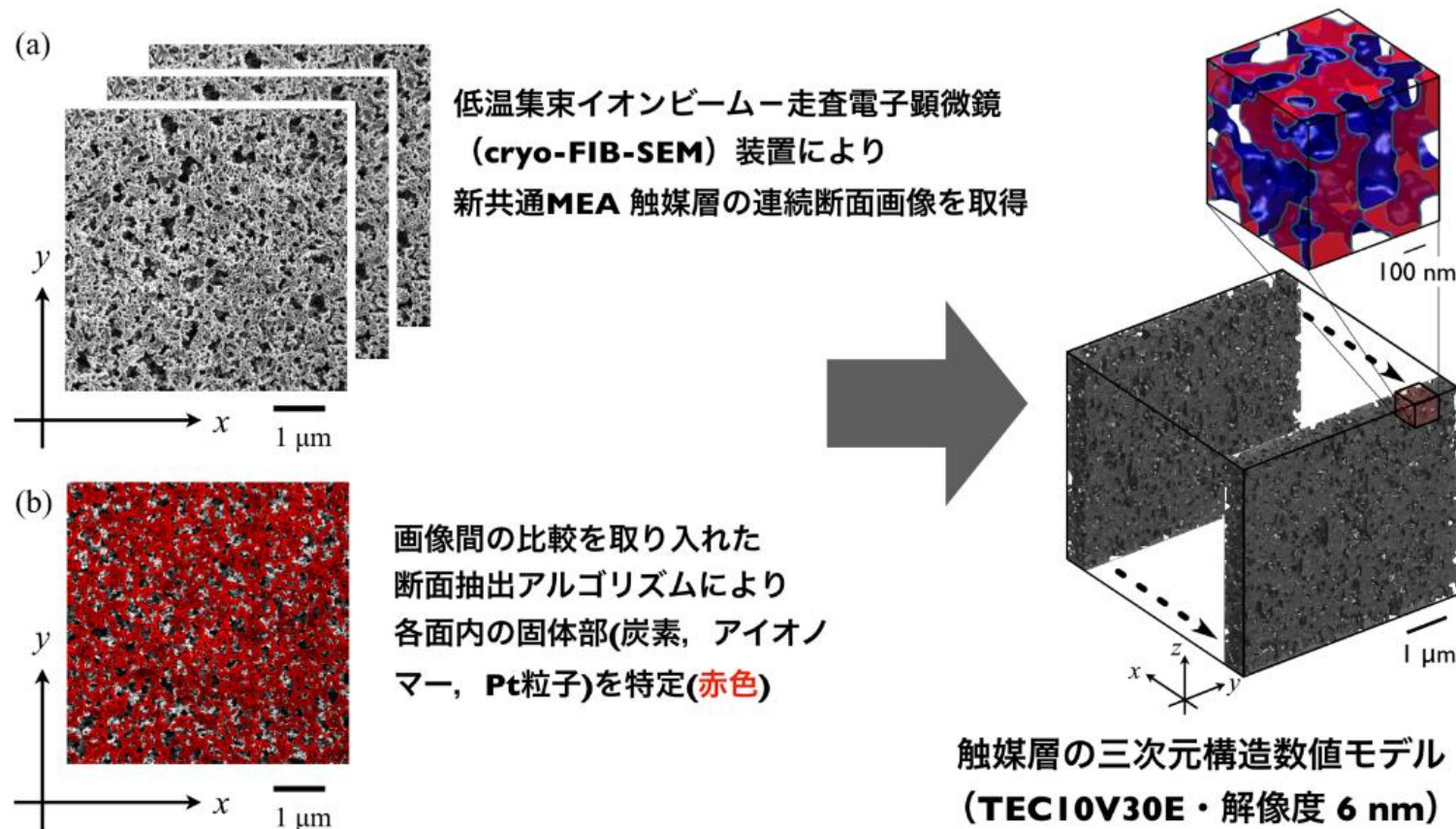
1 μm

● 3D TEM像 (触媒担体粒子)

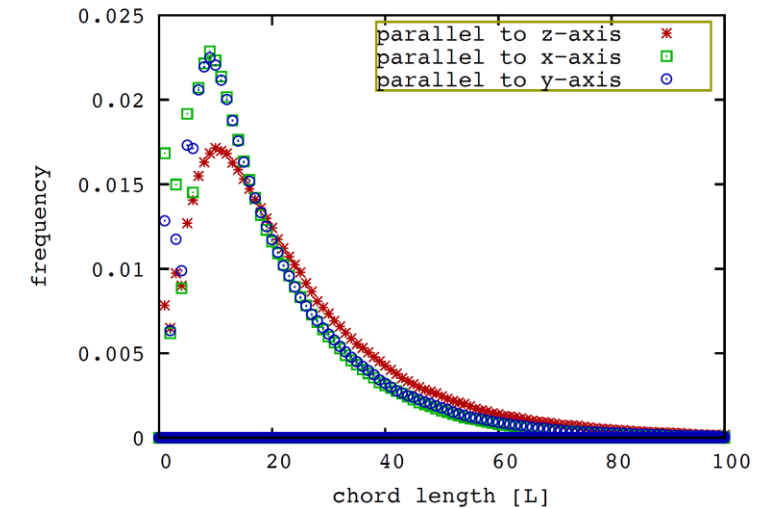


触媒層三次元構造モデルの作成

触媒層のクライオFIB-SEM連続断面画像から
高精度な三次元構造モデルを構築

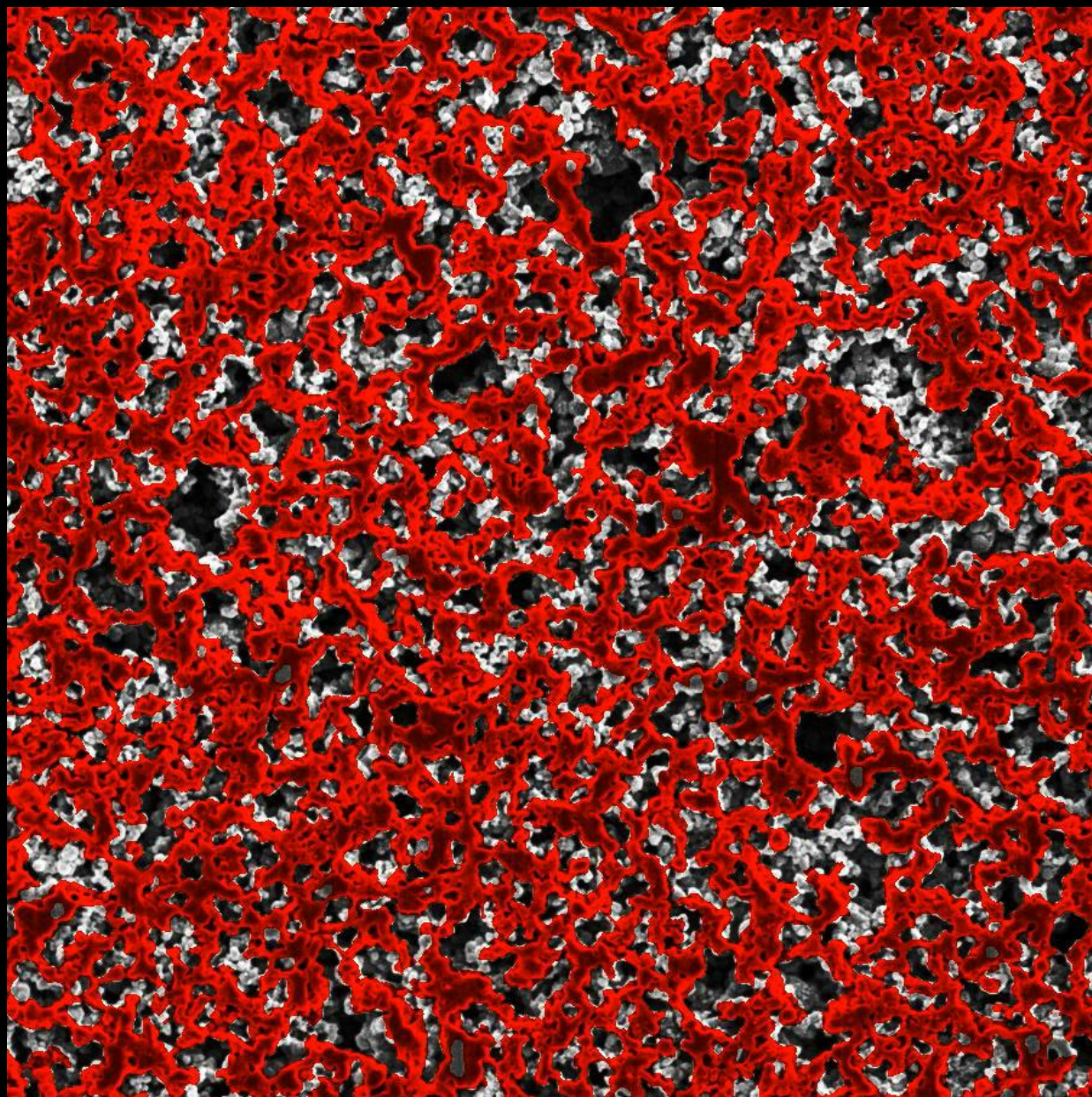


コード長分布



課題

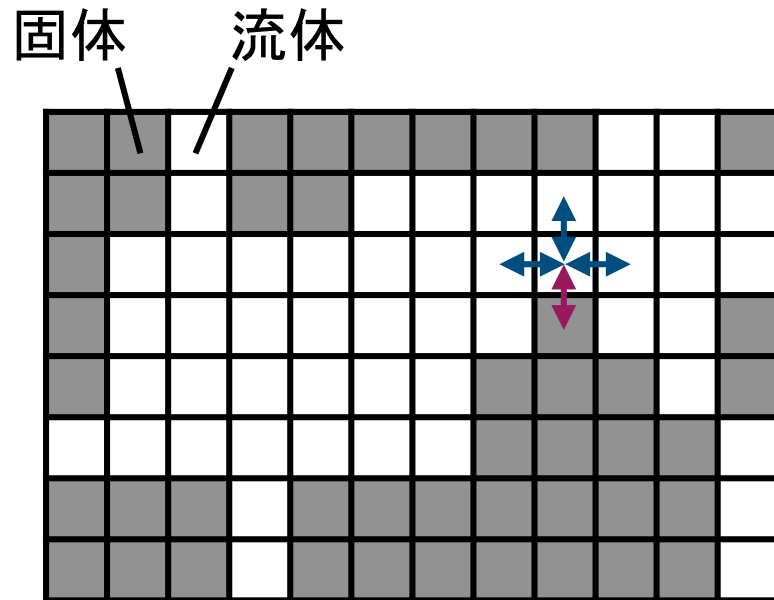
- FIB加工およびSEM観察方向に起因する構造異方性の低減
- アイオノマー被覆分布を含む構造モデルの生成方法の確立



— 1 μm

Y. Yoshimoto, T. Hori, I. Kinefuchi, and S. Takagi, *Phys. Rev. E* **96**, 043112 (2017).

● 格子密度汎関数理論に基づくメソ細孔内の相変化解析



↔ 流体-流体間の相互作用 ϵ_{ff}

↔ 固体-流体間の相互作用 ϵ_{sf}

Helmholtz 自由エネルギーの理想気体成分

$$\Omega(\{\rho\}) = k_B T \sum_i [\rho_i \ln \rho_i + (1 - \rho_i) \ln(1 - \rho_i)]$$

$$- \frac{\epsilon_{ff}}{2} \sum_i \sum_a (1 - \chi(i, a)) \rho_i \rho_{i+a} - \epsilon_{sf} \sum_i \chi(i, a) \rho_i$$

$$- \sum_i \rho_i \mu$$

流体-流体間の相互作用 固体-流体間の相互作用

$a = (\pm 1, 0, 0), (0, \pm 1, 0), (0, 0, \pm 1)$

化学ポテンシャル

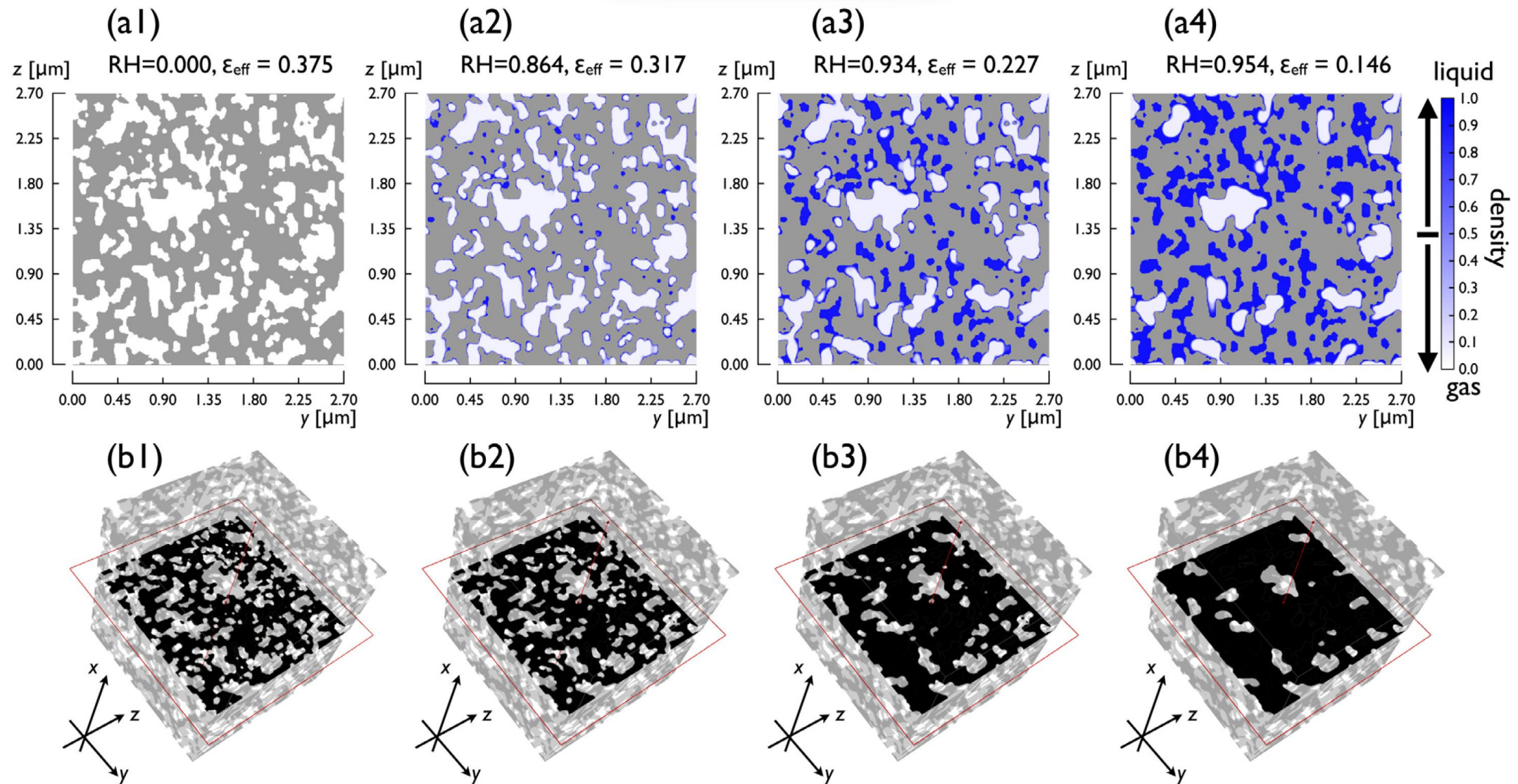
ただし

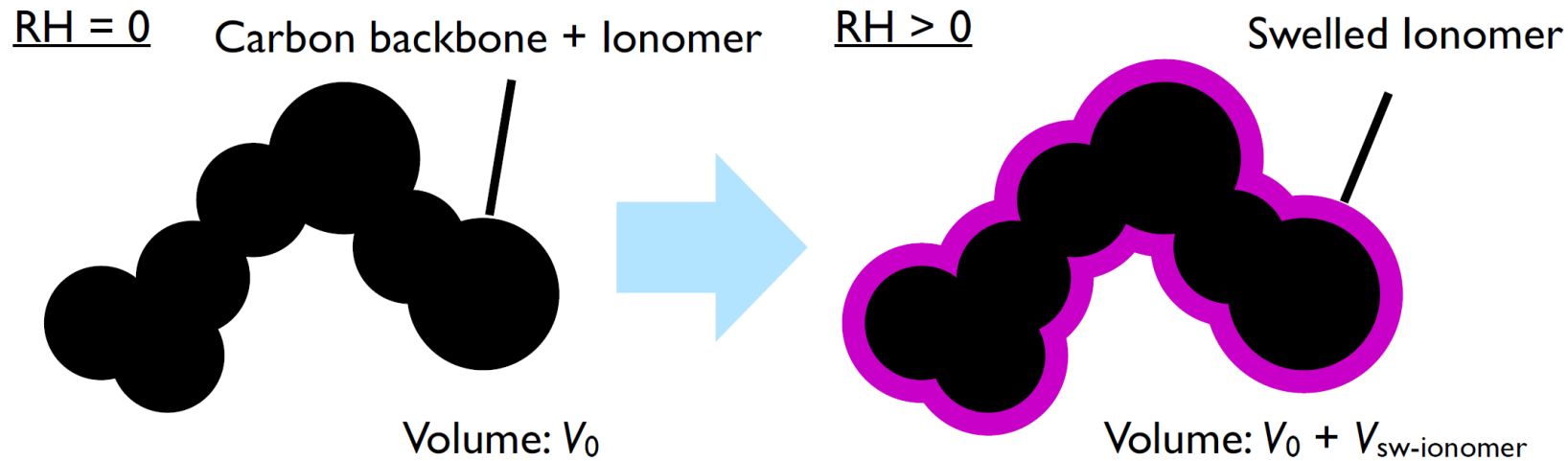
$$\chi(i, a) = \begin{cases} 1 & i+a \text{ が固体のとき} \\ 0 & i+a \text{ が流体のとき} \end{cases}$$

$$\left(\frac{\partial \Omega}{\partial \rho_i} \right)_{\mu, T} = 0 \text{ for } \forall i \text{ となる密度分布が平衡状態に対応}$$

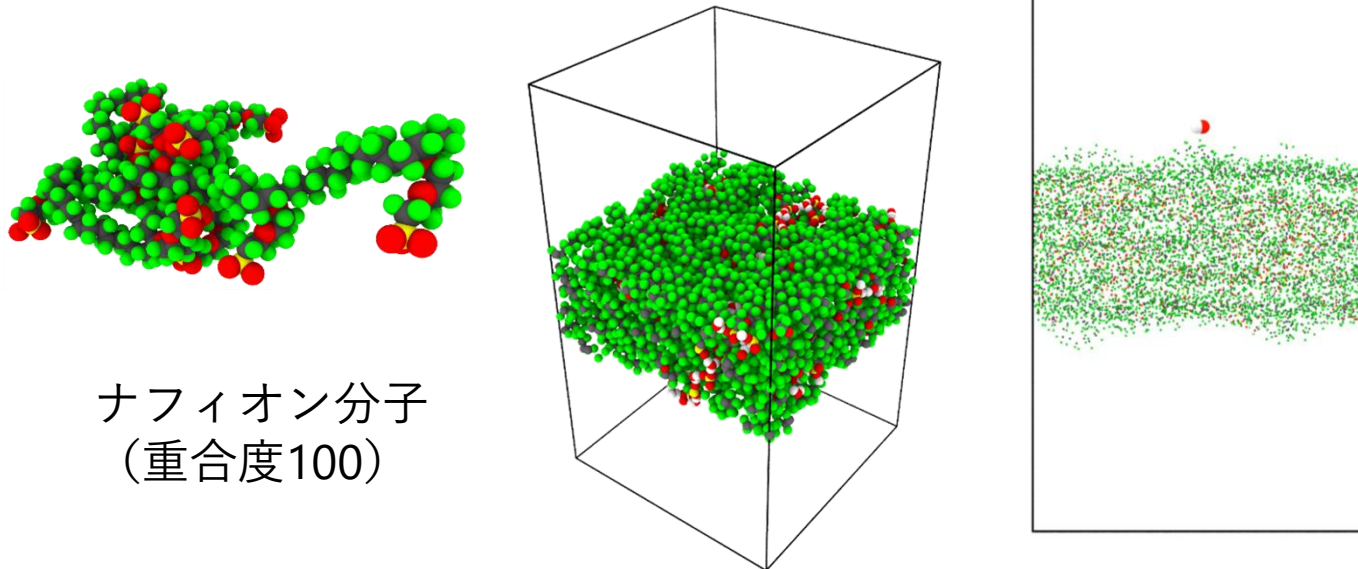
Kelvin式に基づく毛管凝縮モデルが適用できない複雑形状に適用可能

● モンテカルロ法による酸素輸送解析（液水生成構造に対する拡散性評価）





● ナフイオン膨潤のGCMC/MD解析



アイオノマーに関する仮定

- アイオノマーの被覆が均一
 - 固体表面から法線方向に均一に膨潤する
 - 膨潤体積はRHに比例
- $RH = 100\%$ において膨潤体積を0%~40%の範囲で変化させて、酸素輸送特性への影響を評価

触媒層構造

- TEC10V30E, I/C = 1.0

有効拡散係数

$$D_e = \frac{\varepsilon_{\text{eff}}}{\tau} D_0$$

空隙率

屈曲度



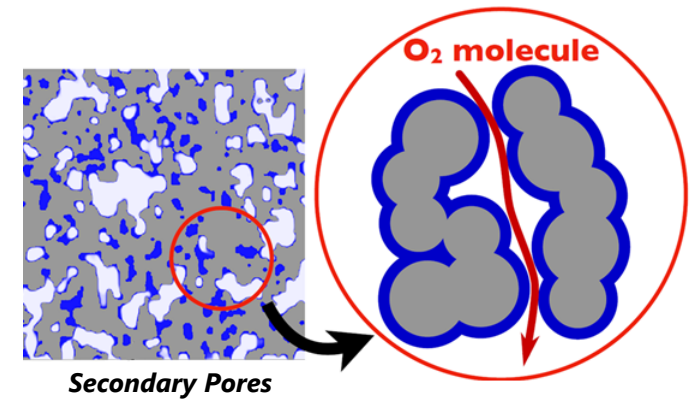
$$\frac{\varepsilon_{\text{eff}}}{\tau} = \frac{D_e(\text{Kn} = \infty)}{D_0(\text{Kn} = \infty)} = \frac{D_e^\infty}{D_K} \quad \left. \vphantom{\frac{D_e^\infty}{D_K}} \right\} \text{Monte-Carlo Simulations}$$

D_e^∞ , the effective diffusion coefficient in the Knudsen regime can be evaluated using mean-square displacement (MSD):

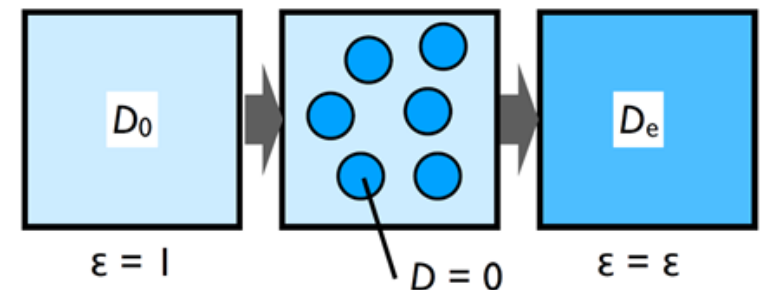
$$D_e^\infty = \varepsilon_{\text{eff}} \lim_{t \rightarrow \infty} \frac{\langle |\mathbf{r}(t) - \mathbf{r}(0)|^2 \rangle}{6t}$$

D_K , the Knudsen diffusion coefficient can be evaluated from

$$D_K = \frac{v}{3} \left(\frac{\langle l^2 \rangle}{2\langle l \rangle^2} - \beta \right) \langle l \rangle$$



Knudsen Diffusion and Monte Carlo Simulation

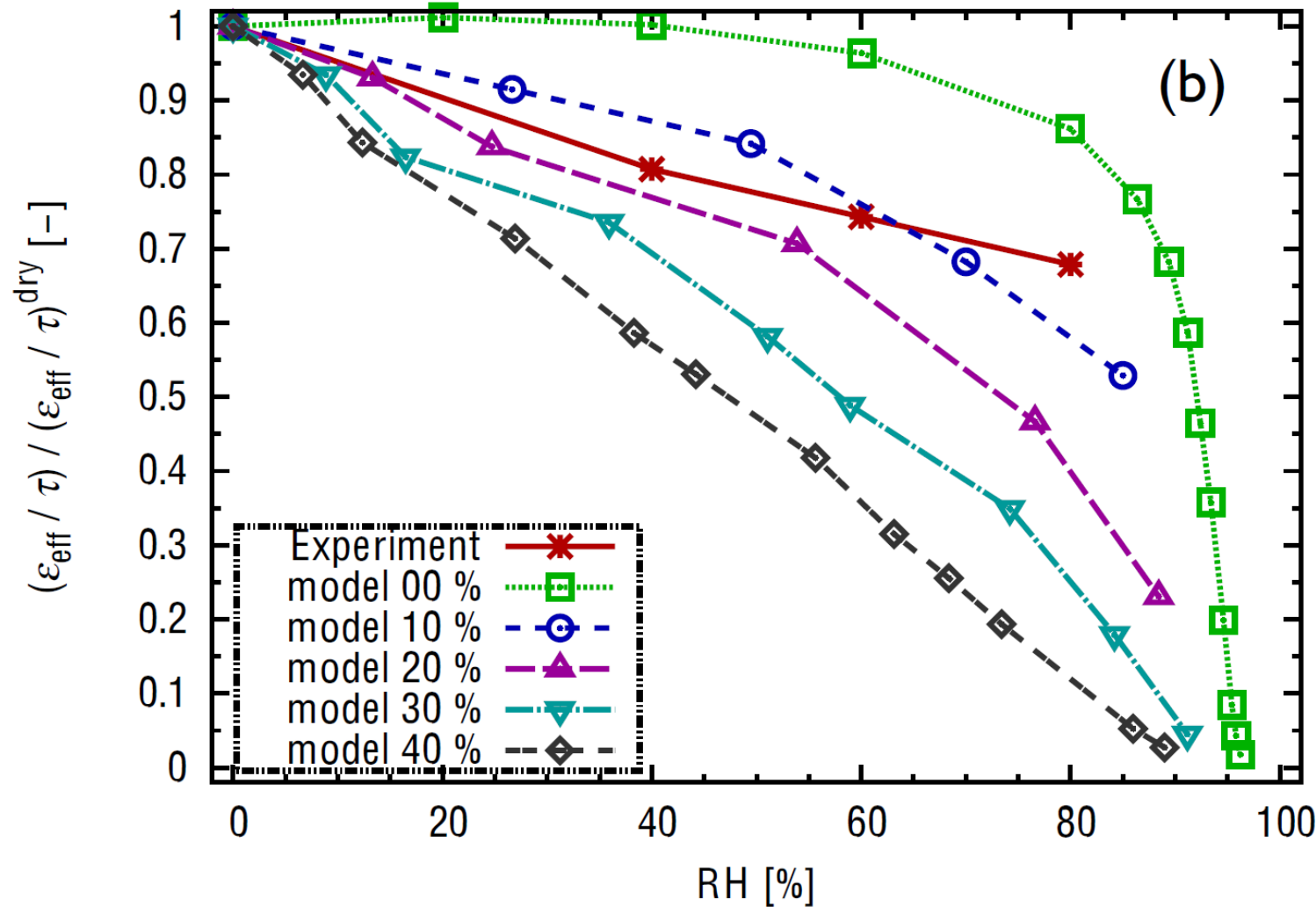


Bruggeman correlation

[V. D. Bruggeman, Ann. Phys., 1935]

$$\frac{\varepsilon}{\tau} = \frac{D_e}{D_0} = \varepsilon^a$$

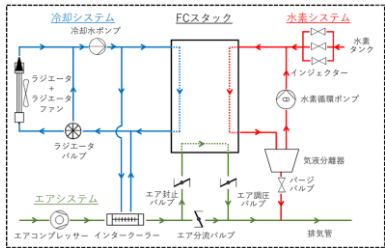
$a=1.5$ (spheres)
 $a=2$ (cylinders)



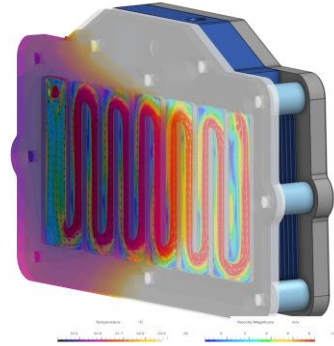
- 乾燥条件 (RH=0%) の $\varepsilon_{\text{eff}}/\tau$ からの相対変化で評価
- アイオノマー膨潤体積 10% @RH=100% のモデルが実験結果と比較的良く一致

Multi-physics

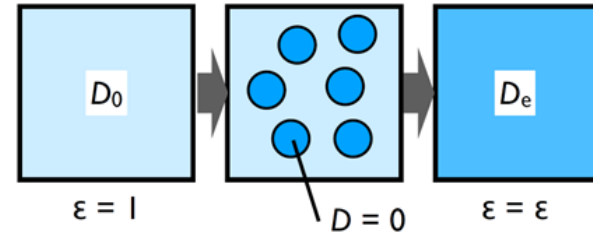
FC•DynaMo



<https://www.ch.t.kyoto-u.ac.jp/ja/information/laboratory/3koza/fc-dynamo>



<https://www.simscale.com/blog/hydrogen-fuel-cell-simulation-and-modeling/>



Bruggeman correlation

[V. D. Bruggeman, Ann. Phys., 1935]

$$\frac{\epsilon}{\tau} = \frac{D_e}{D_0} = \epsilon^a$$

$a=1.5$ (spheres)
 $a=2$ (cylinders)

$$\Omega(\{\rho\}) = k_B T \sum_i [\rho_i \ln \rho_i + (1 - \rho_i) \ln(1 - \rho_i)] V_i$$

Ideal Gas Contribution

$$-\frac{\epsilon_{ff}}{2} \sum_i \sum_{a \leq r_c} \rho_{i+a} \rho_i V_i$$

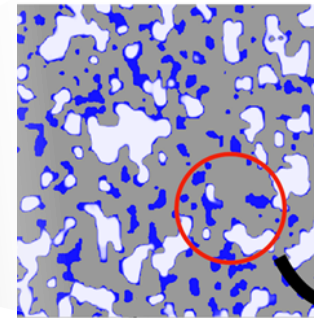
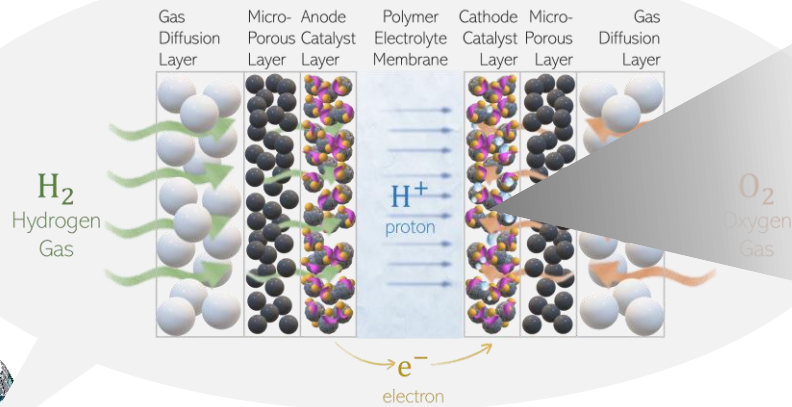
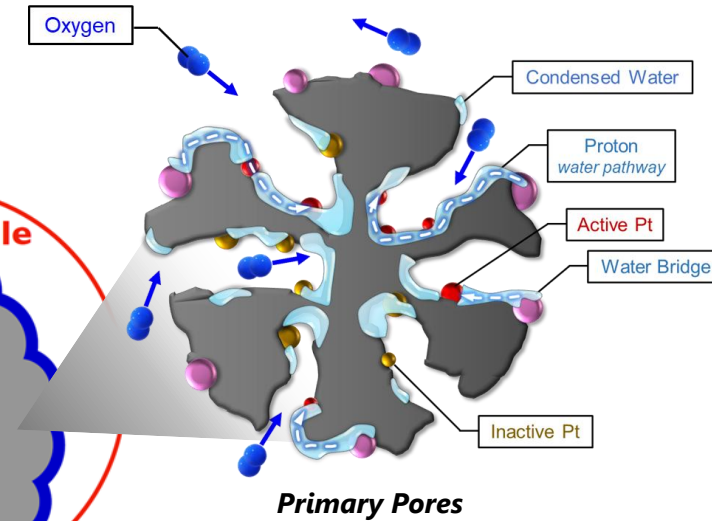
Fluid-Fluid Interaction

$$-\epsilon_{sf} \sum_i \sum_{|a| \leq r_c} \chi(i, a) \rho_i V_i$$

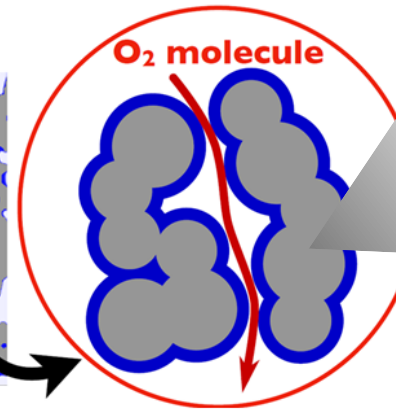
Solid-Fluid Interaction

$$-\sum_i \mu \rho_i V_i$$

Chemical Potential

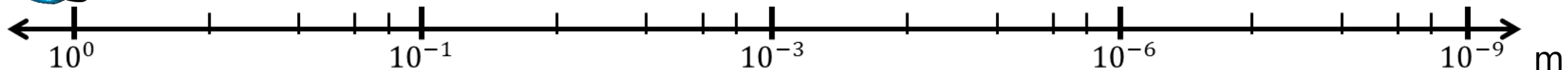


Secondary Pores



O₂ molecule

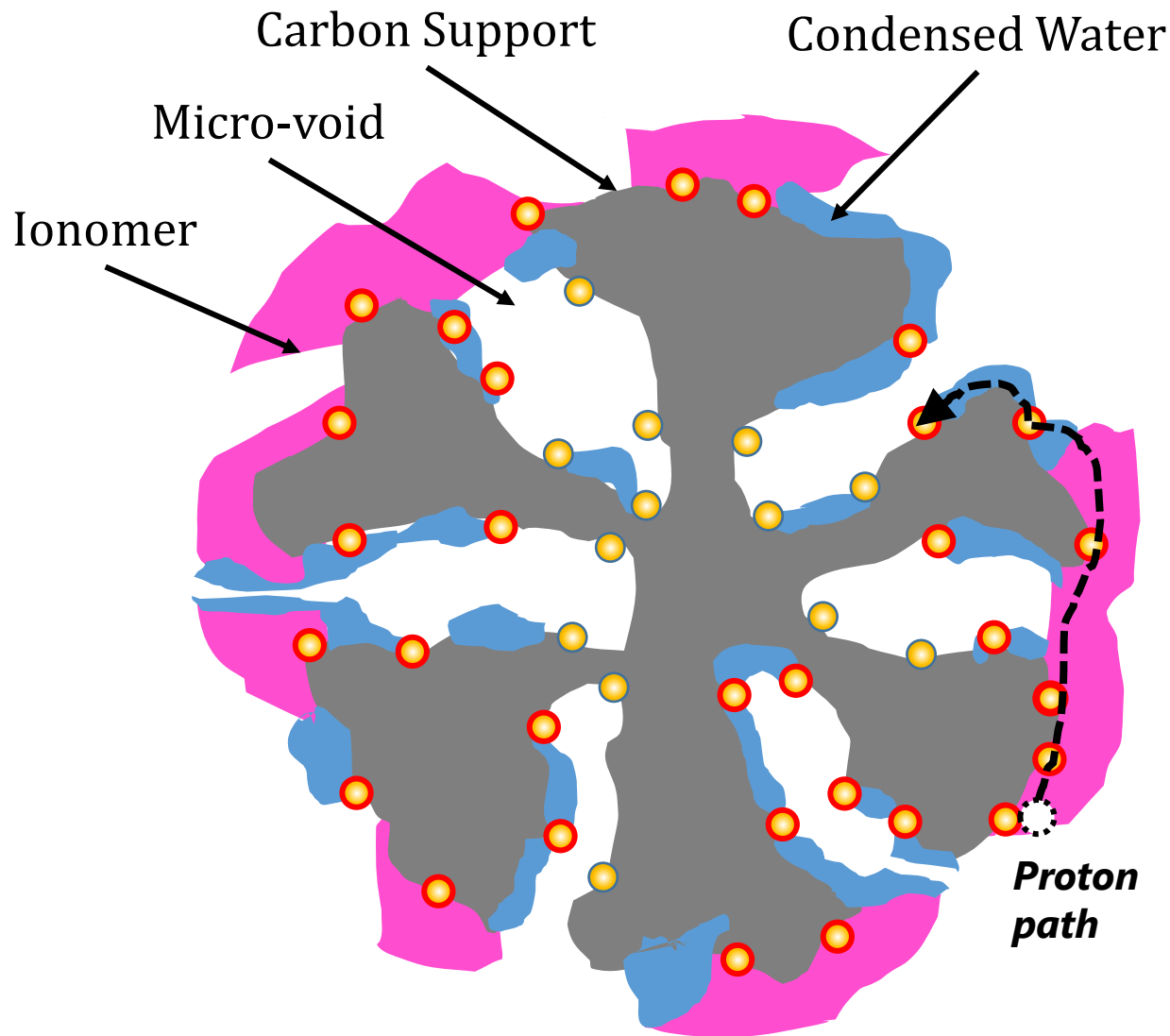
Multi-scale



多孔性触媒担体内部の白金利用率の変化

11

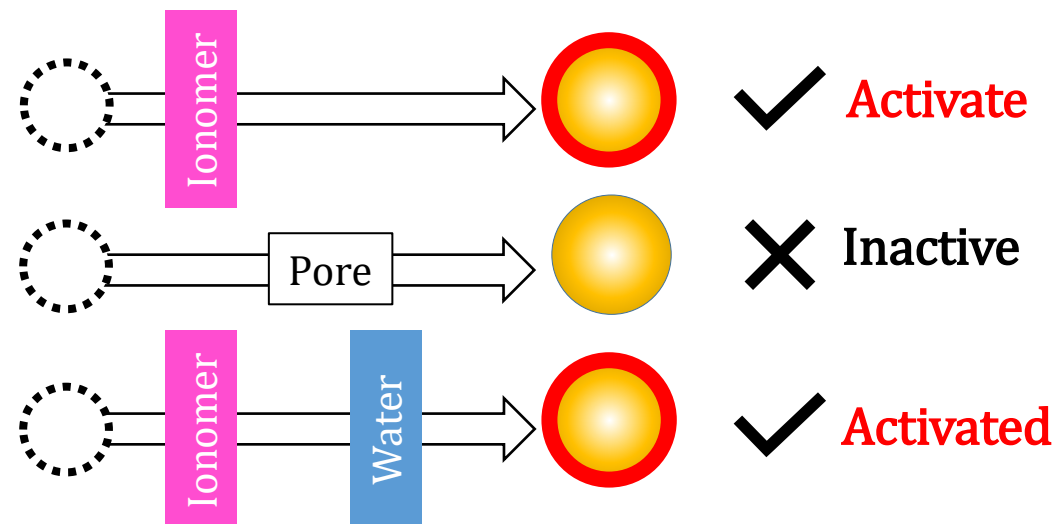
電気化学的表面積（ECSA：Electrochemical surface area）



 Platinum Particle (**Active**)
in-contact with ionomer

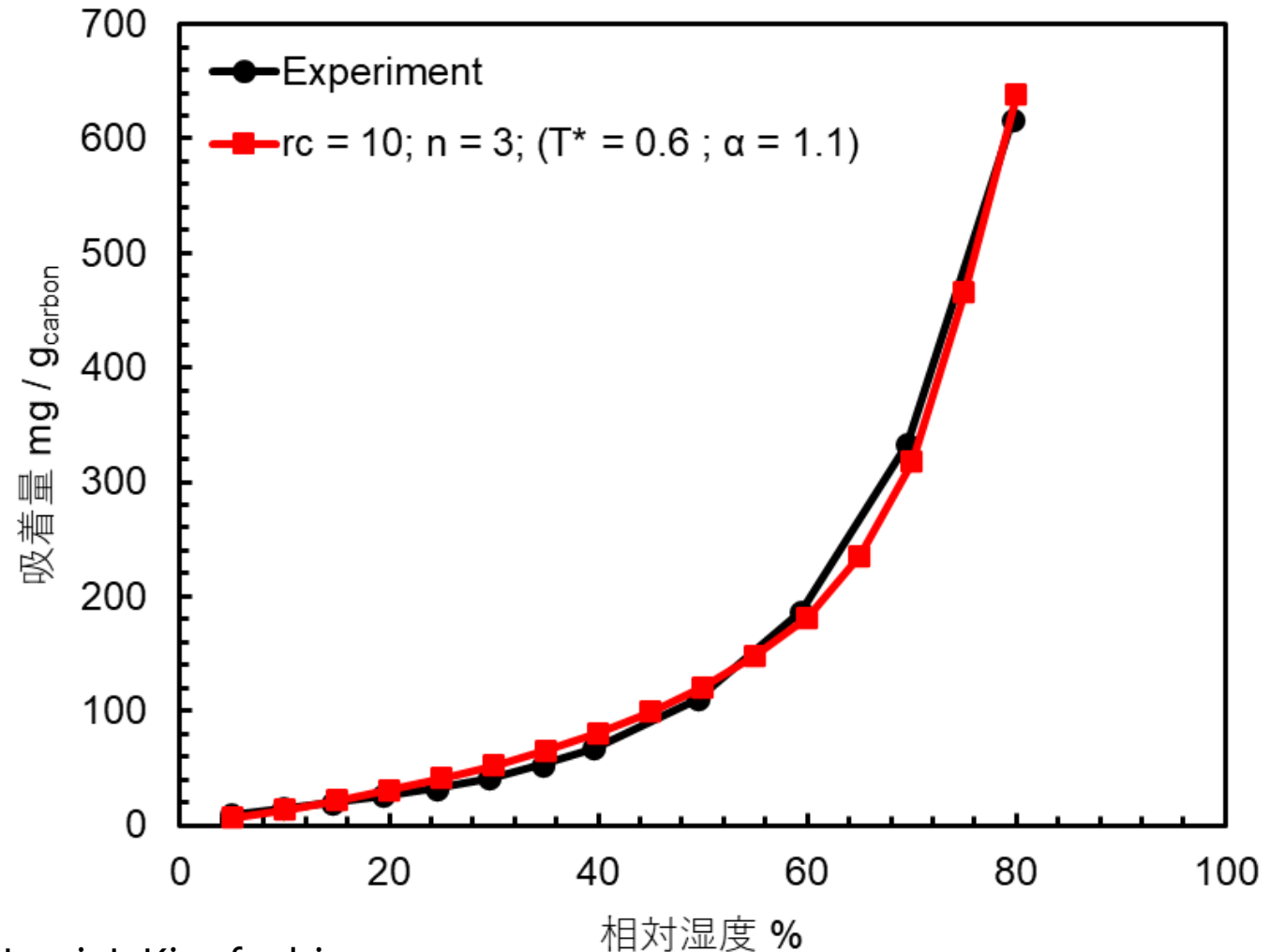
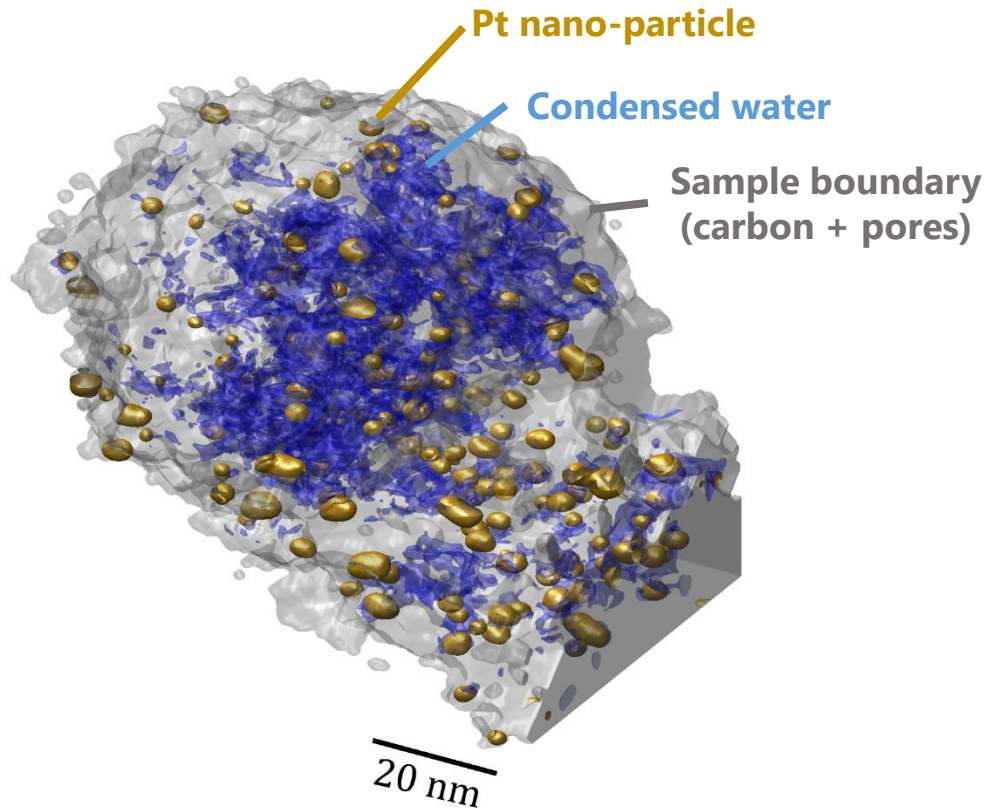
 Platinum Particle (**Inactive**)
no contact with ionomer

Proton Pathway



LDFT Simulation

トヨタMIRAI（第2世代）のカソード触媒層材料を対象

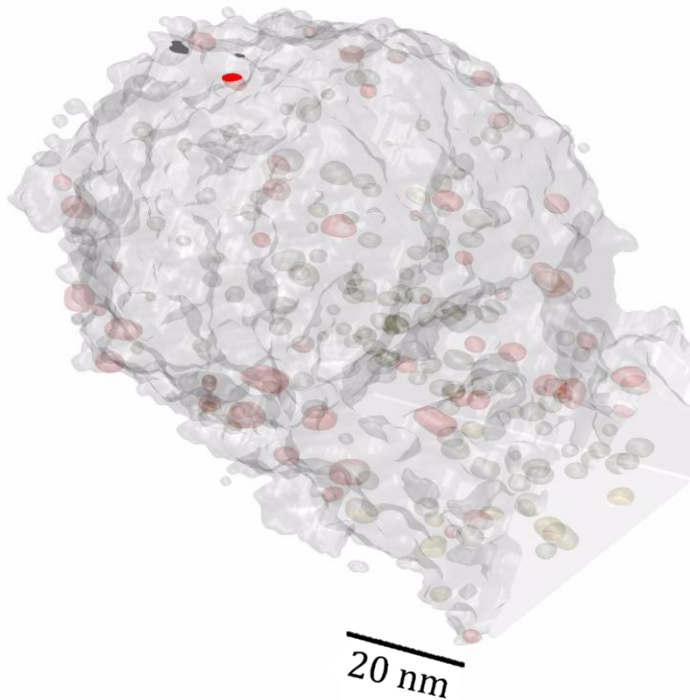


C. Otic, S. Katayama, M. Arao, M. Matsumoto, H. Imai, I. Kinefuchi,
ACS Applied Materials & Interfaces **16** (16), 20375 (2024).

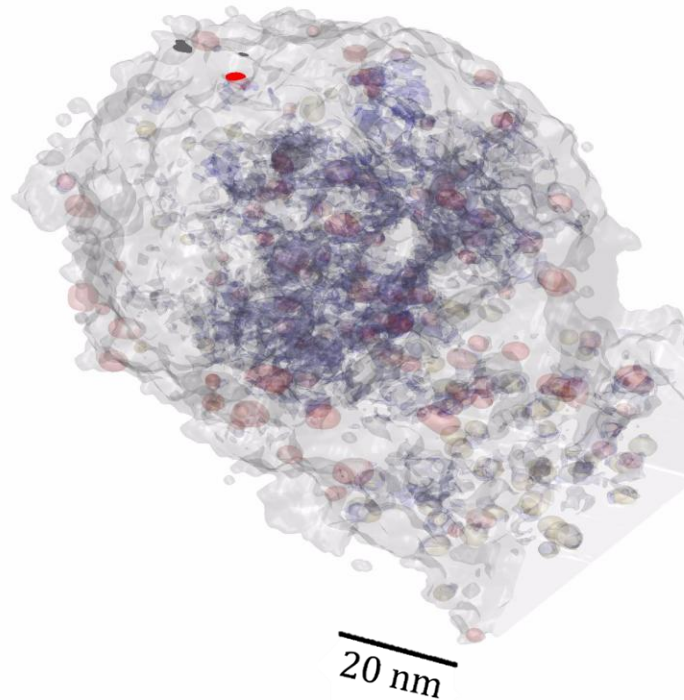
Pt utilization based on LDFT simulation (Wet)

The goal is to evaluate whether Pt nanoparticles **"have access"** to the surface of the particle through **"water bridges"**.

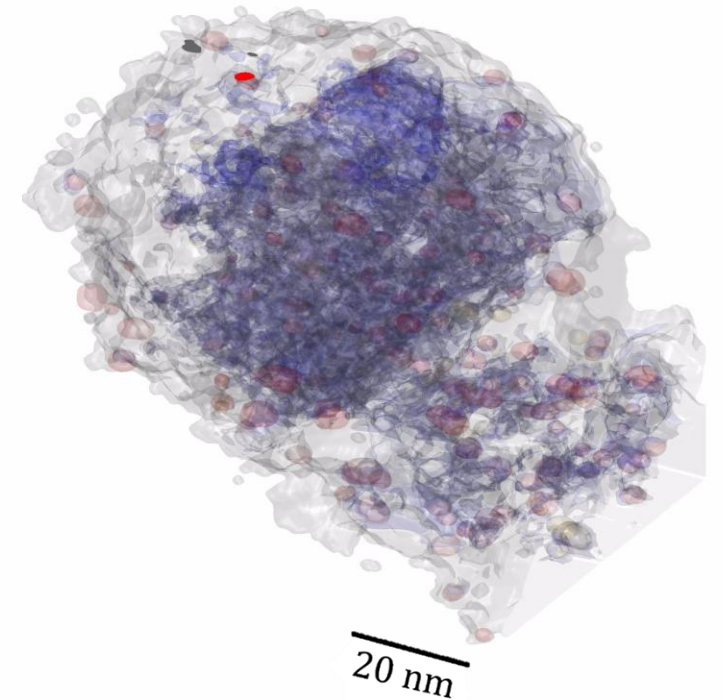
- Inactive Platinum
- Active Platinum
- Sample Boundary (Carbon + Pore)
- Condensed Water



RH = 00%
Active Pt = 28%



RH = 60%
Active Pt = 62%



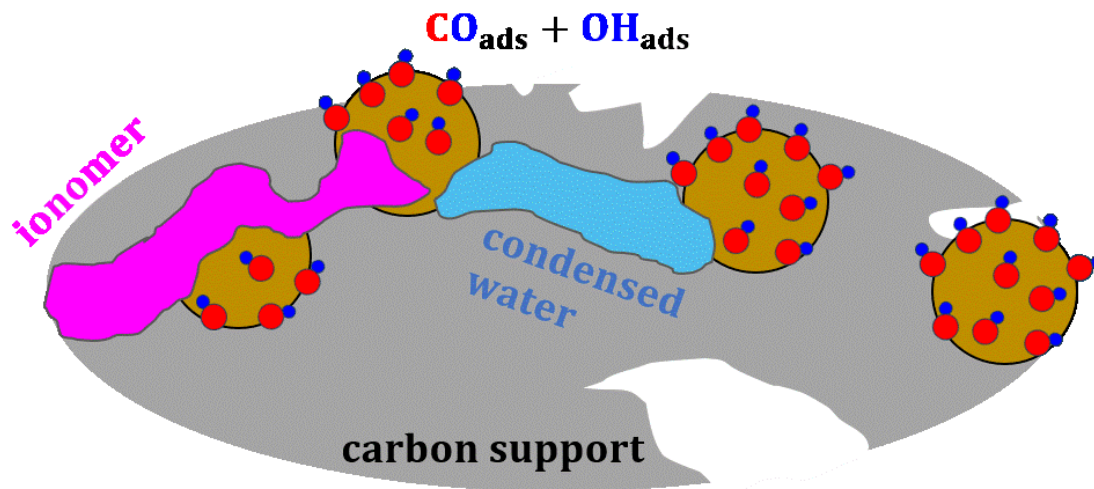
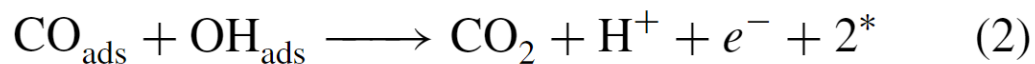
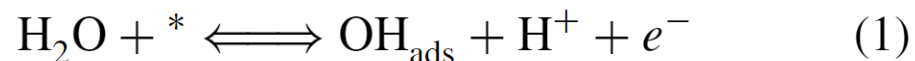
RH = 80%
Active Pt = 87%

白金利用率

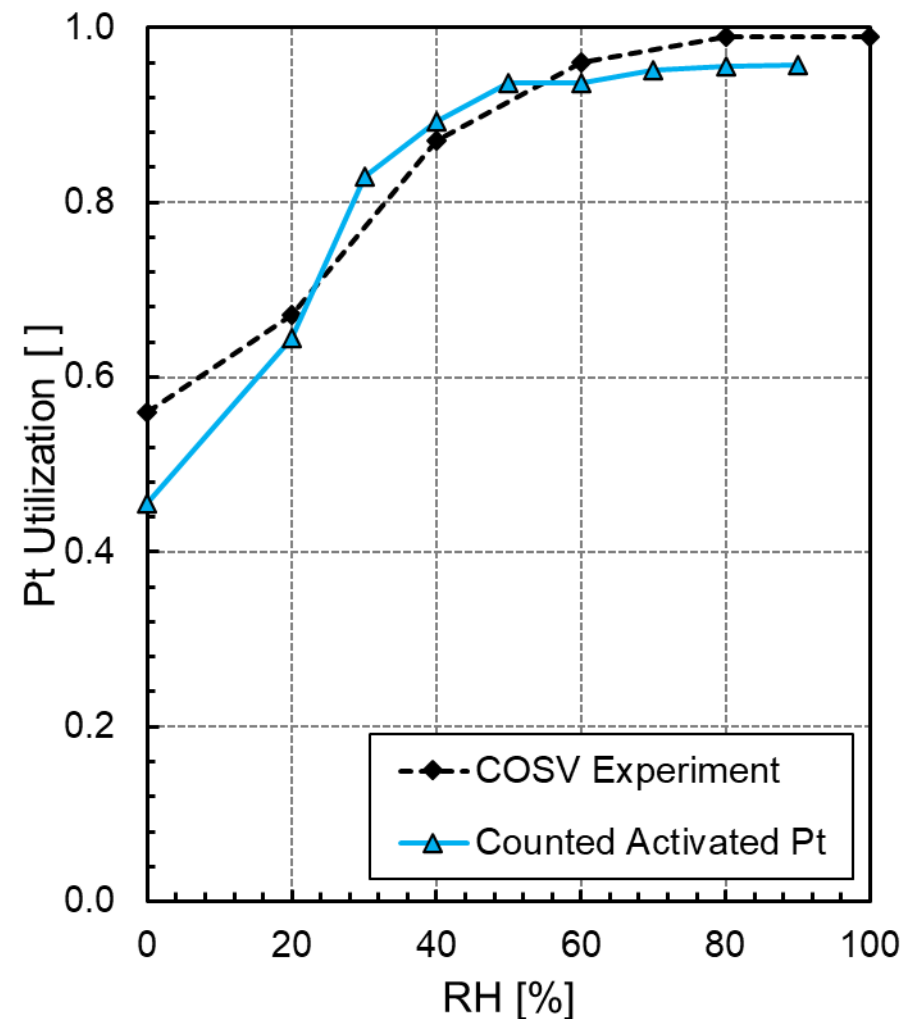
多孔性触媒担体「内部」の白金利用率の湿度依存性の説明に成功

Comparison with Carbon Monoxide Stripping Voltammetry (COSV)

*ECSA by electrooxidation of adsorbed
CO monolayer on the catalyst surface.*



Pt Catalyst Activation



実材料の三次元構造データを用いて、カソード触媒層内の水の相変化、酸素拡散、プロトン伝導を評価するシミュレーションツールを構築

対象：触媒担体粒子内の細孔（数nm），二次細孔（数十nm～数 μm ）

手法：格子密度汎関数法 (相変化), 気体拡散 (希薄気体力学), 画像処理 (断面抽出)

実験結果の理解，材料設計指針の提示

- C. Otic et al., ACS Appl. Mater. Interfaces 16, 20375 (2024).
- T. Kaneko et al., Int. J. Heat Mass Transf. 200, 123491 (2022).
- S. Shimotori et al., Phys. Rev. E 104, 045105 (2021).
- T. Kaneko et al., Int. J. Heat Mass Transf. 150, 119277 (2020).
- M. Nakauchi et al., J. Phys. Chem. C 123, 7125 (2019).
- T Hori et al., Phys. Rev. E 97, 013101 (2018).
- Y. Yoshimoto et al., Phys. Rev. E 96, 043112 (2017).
- A. Fukushima, J. Phys. Chem. C 119, 28396 (2015).

